



# RAYLEIGH-BÉNARD INSTABILITY OF THE POWER-LAW FLUID FLOW IN A POROUS MEDIUM: NUMERICAL AND EXPERIMENTAL ANALYSIS

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## THEORETICAL ANALYSIS

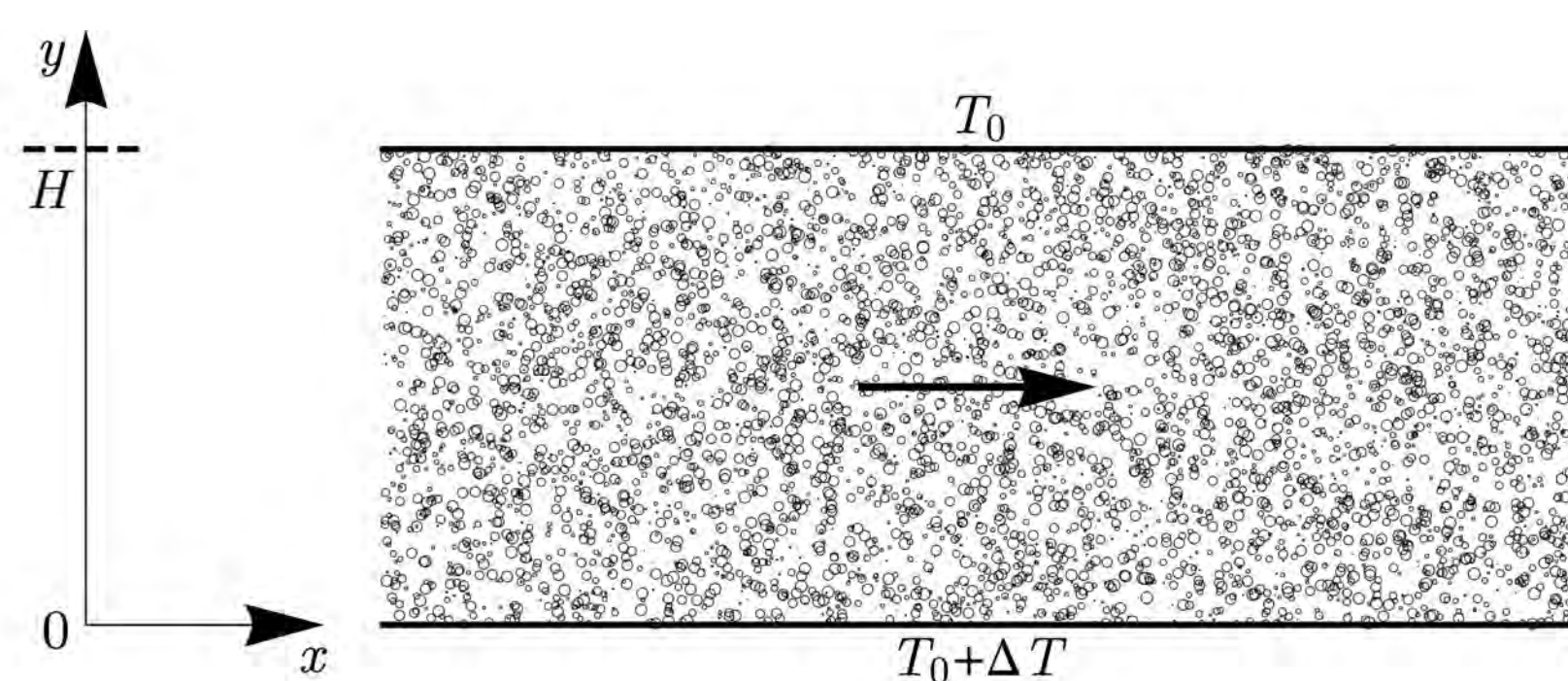
The linear stability of fluid a saturated porous channel heated from below is studied. The governing equations are the following

$$\begin{aligned} \nabla \cdot \mathbf{u} &= 0 \\ \frac{\mu^*(T)}{K} |\mathbf{u}|^{n-1} \mathbf{u} &= -\nabla p - \rho_0 \mathbf{g} \beta (T - T_0) \\ \sigma \frac{\partial T}{\partial t} + \mathbf{u} \cdot \nabla T &= \varkappa \nabla^2 T \\ y = 0 : \quad v = 0, \quad T &= T_0 + \Delta T \\ y = H : \quad v = 0, \quad T &= T_0 \end{aligned}$$

The consistency index of the power law fluid depends on temperature

$$\mu^*(T) = \mu_0^* [1 + \xi (T - T_0)]^{-n}$$

Where  $\xi$  is a fluid property modulating the slope of the temperature change of the consistency index.

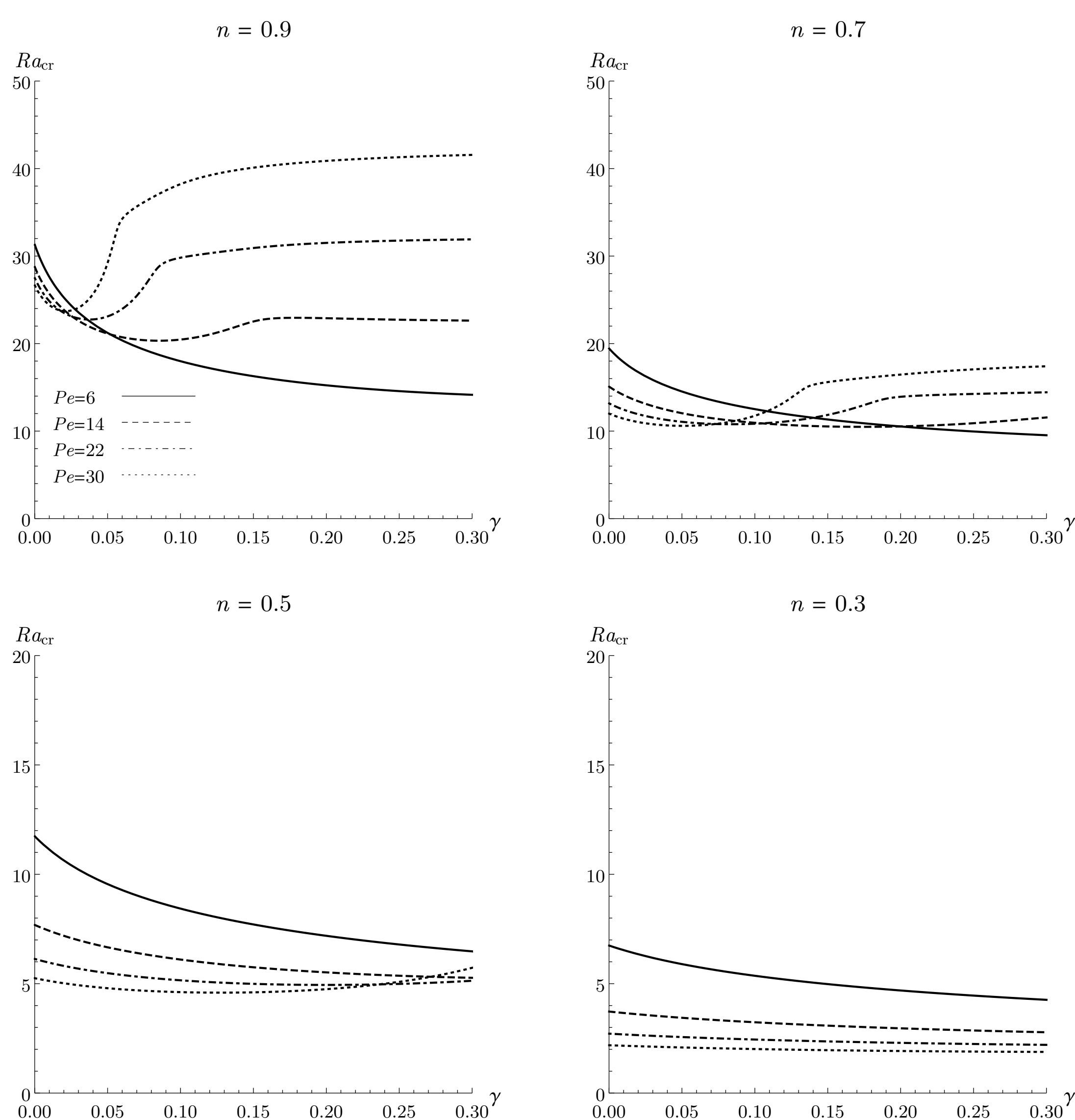


Geometry of the fluid a saturated porous channel

A two dimensional,  $(x, y)$ , configuration is studied.

## RESULTS

The stability analysis consists in finding the critical values that identify the threshold conditions for the onset of convective instability.



Critical values of the governing parameter  $Ra$

Where the governing parameter here are the Rayleigh number  $Ra$ ,  $\gamma$  a non-negative dimensionless parameter that tunes the departure from the constant consistency index model and the Péclet number  $Pe$

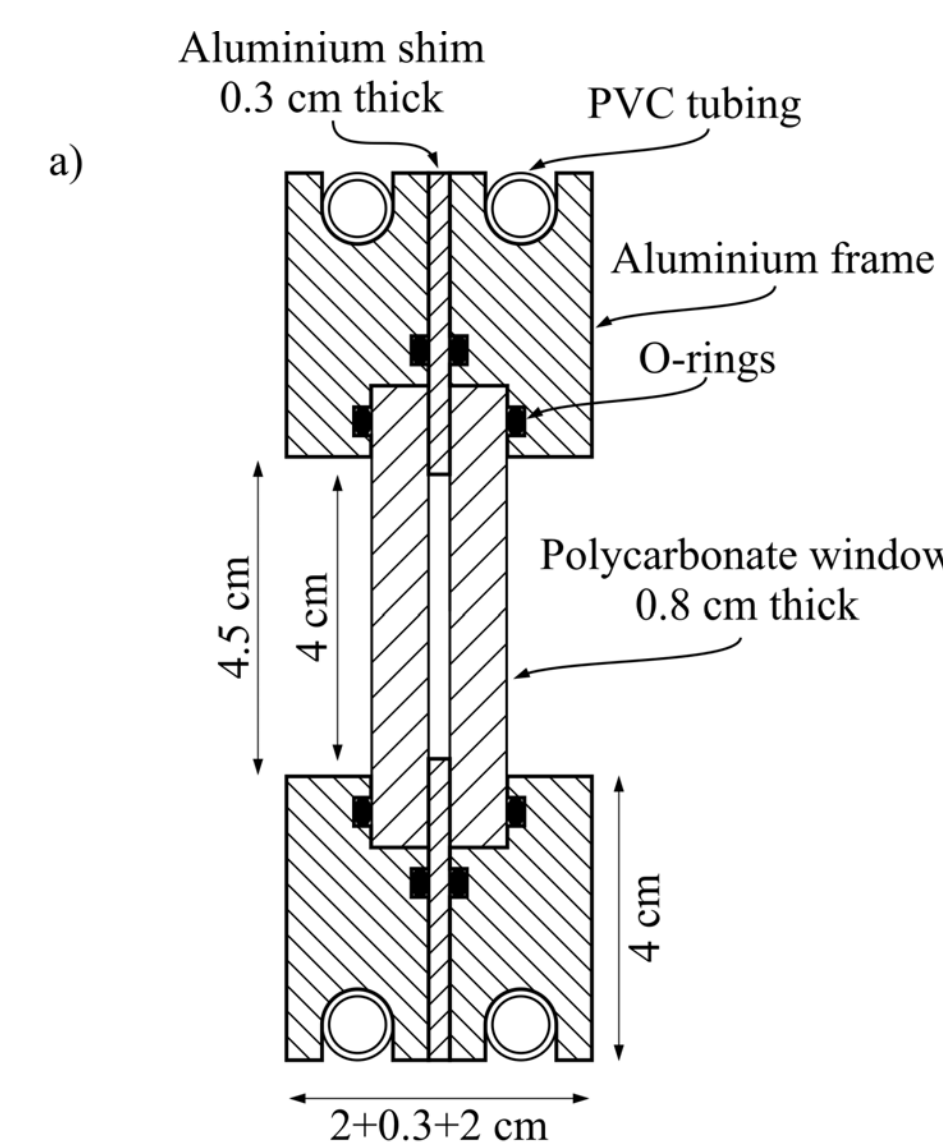
$$Ra = \frac{\rho_0 g \beta \Delta T K H^n}{\mu_0^* \varkappa^n} \quad \gamma = \frac{\mu_0^* \varkappa^n \xi}{\rho_0 g \beta K H^n} \quad Pe = \frac{u_0 H}{\varkappa}$$

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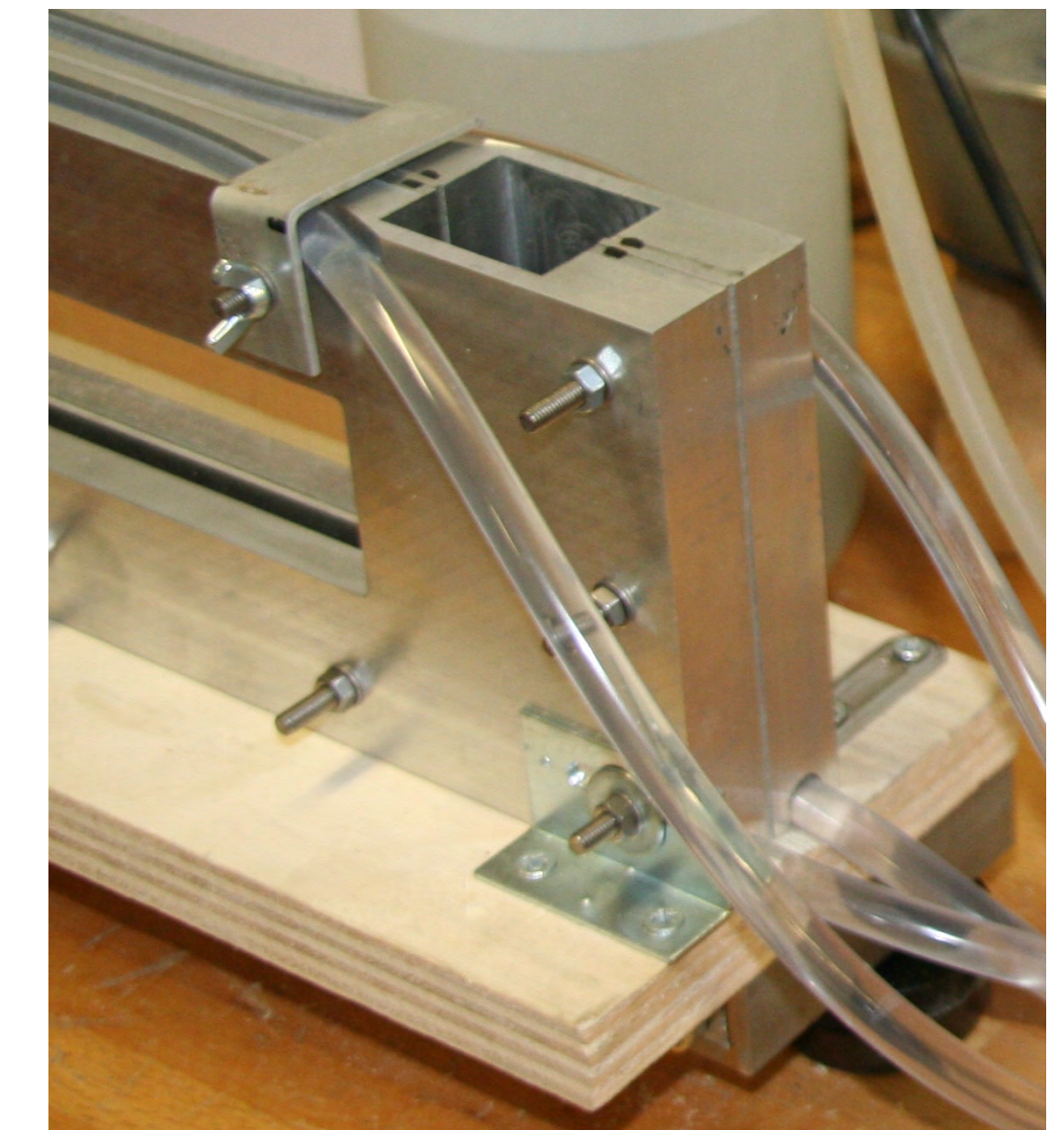
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## EXPERIMENTAL ANALYSIS

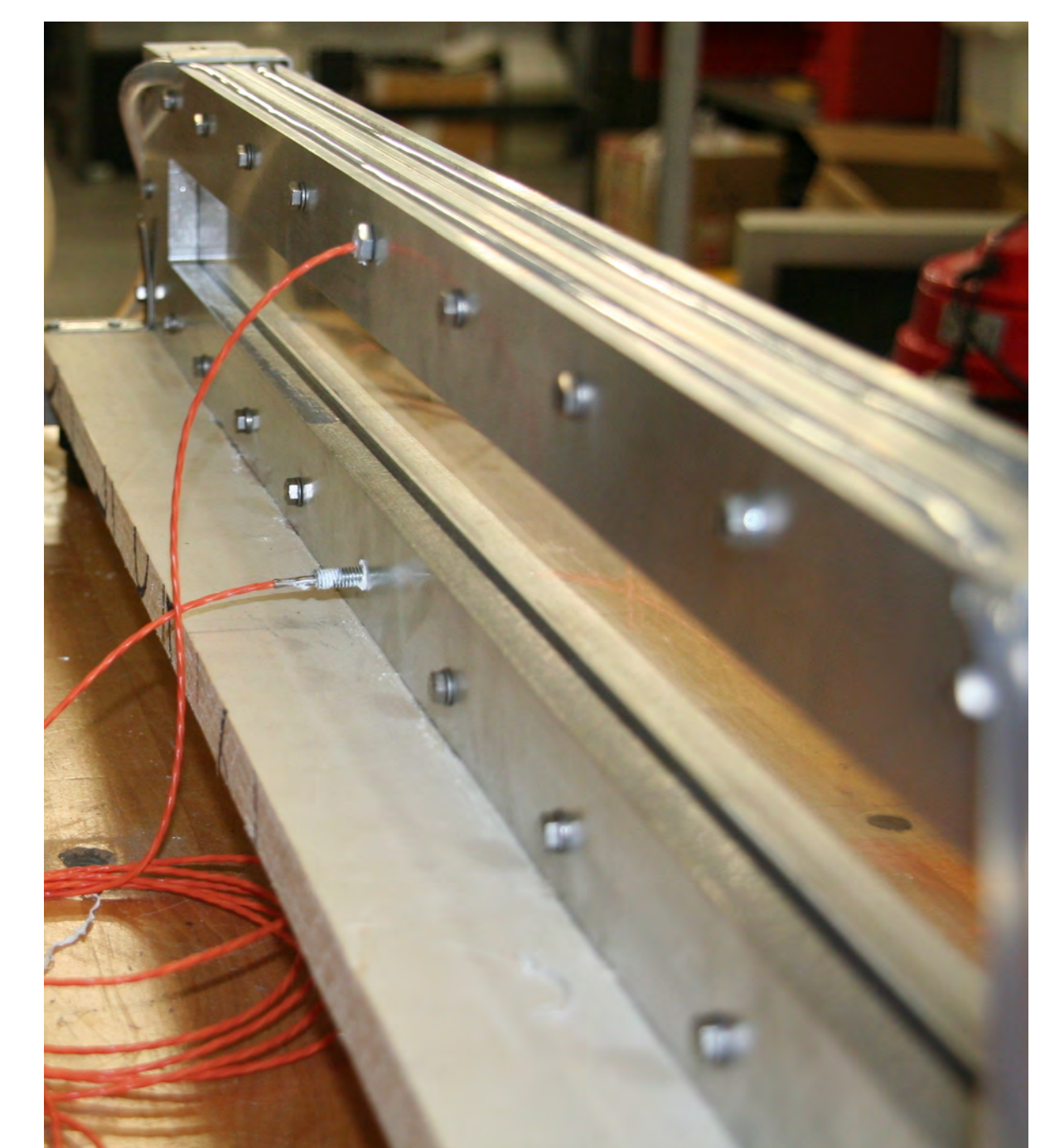
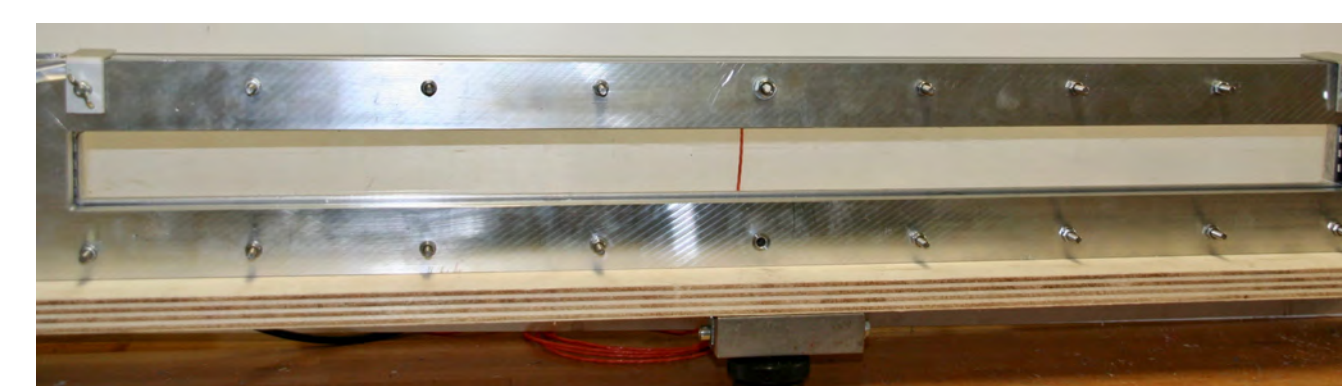
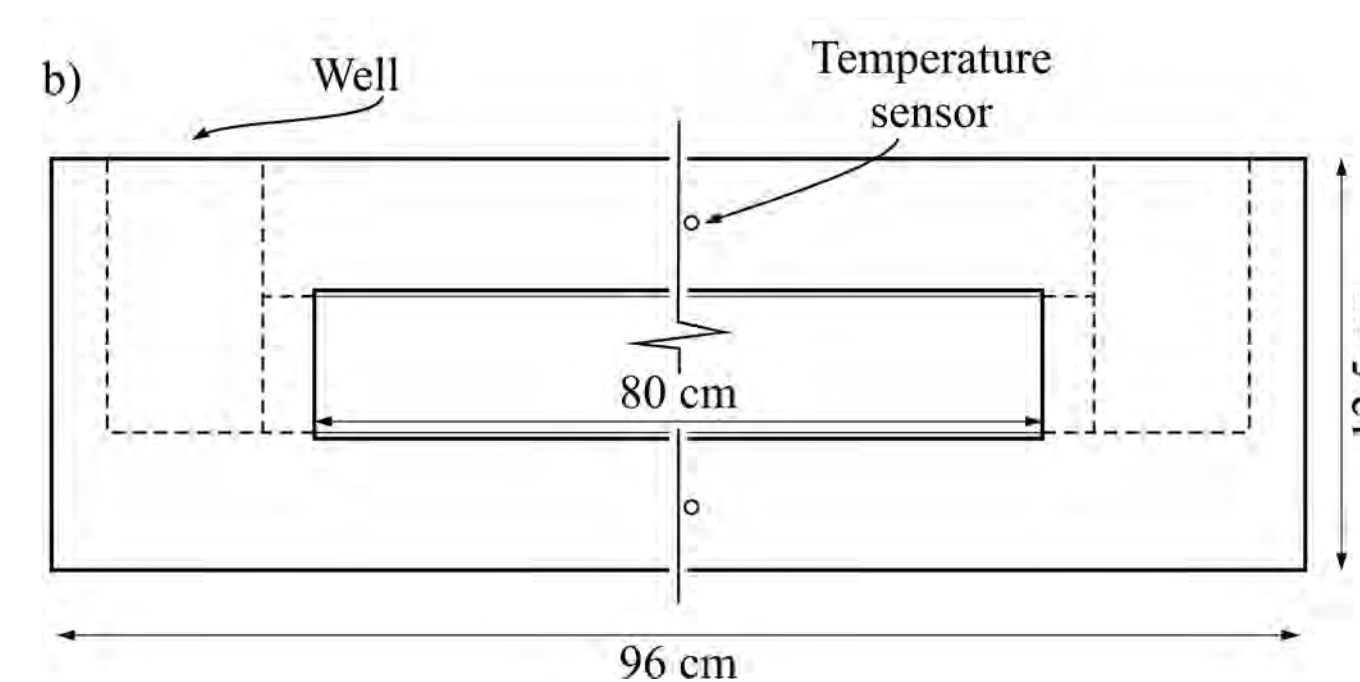
The two dimensional behaviour of the fluid saturated porous medium is simulated experimentally by employing a Hele-Shaw cell of length  $L = 80$  cm and height  $H = 4$  cm similar to Hartline and Lister (1977)



Cross-section of the Hele-Shaw cell



The optical access is through two polycarbonate windows 0.8 cm thick, with a gap maintained by aluminium shims of 0.1, 0.2, and 0.3 cm. The assembly is held together by an aluminium frame machined by using a CNC milling cutter. The temperature control is obtained by circulating water at the hot lower side, and coolant at the cold upper side.



Front and view of the Hele-Shaw cell

The rheology of the fluid was measured with a parallel plate rheometer (Dynamic Shear Rheometer Anton Paar Physica MCR 101), and the mass density with a hydrometer (STV3500/23 Salmoiraghi), with an accuracy of 1%.

## PRELIMINARY RESULTS

The flow visualization is obtained by injecting a colored ink inside the cell. This method does not affect the flow features.



Temperature difference  $\Delta T = 16.3$  K



Temperature difference  $\Delta T = 10.4$  K

Preliminary results show that the convective instability arises for values of Rayleigh number compatible with those obtained by the numerical analysis.